

Iraqi Journal of Chemical and Petroleum Engineering Vol.14 No.3 (September 2013) 55- 62 ISSN: 1997-4884



Removal of Phenolic Compounds from Aqueous Solution by Using Agricultural Waste (Al-Khriet)

Hayder A.K. Al-jandeel

Chemical Engineering Department, College of Engineering, University of Baghdad

Abstract

Adsorption techniques are widely used to remove organics pollutants from waste water particularly, when using low cost adsorbent available in Iraq. Al-Khriet powder which was found in legs of Typha Domingensis is used as bio sorbent for removing phenolic compounds from aqueous solution. The influence of adsorbent dosage and contact time on removal percentage and adsorb ate amount of phenol and 4- nitro phenol onto Al-Khriet were studied. The highest adsorption capacity was for 4- nitrophenol 91.5% than for phenol 82% with 50 mg/L concentration, 0.5 gm. dosage of adsorbent and pH 6 under a batch condition. The experimental data were tested using different isotherm models. The results show that Freundlich model resulted in the best fit also the kinetic study make it clear that the adsorption process proceeded according to the pseudo second order model.

Key Words: Al-Khriet, Agricultural waste adsorbent, Bio sorption, phenolic compound, isotherm kinetic model

Introduction

Phenols and their derivatives are known to be highly toxic for human beings and the aquatic life [1]. They industrial result from different processes such as, synthetic rubber, petrochemical industry, plastics, coking. paper, phenolic resin industries, and oil refineries [2, 3]. The use of water contained phenol can result in retardation of the central nervous system (CNS), impairment of the liver, kidney and irritation of the eyes, skin and mucous membrane [4]. It had been concluded from earlier studies that the skin is a route of entrance of phenol [5]. A 32 years old man died soon after spilling strong solution of phenol above his shoulder and other part of his body. Chronic

phenol poisoning is diagnosed by the disfunction of different body system such as the nervous system. The human eyes is very sensitive to the chemical especially the phenol causing swelling and burns as well as the cornea may become white or even loosen sensation. Loss of vision has happened in some case [6]. According to the world health organization (WHO), the recommended concentration of phenolic compound in drink water is 1 mg/L [7] and that is why it is strongly recommended to remove phenolic compounds from wastewater. For this reason different environment friendly process had been used. Several physicochemical and biological treatment techniques such as chemical oxidation [8], ultrasonic degradation [9], photo catalytic degradation using son photo chemical [10], enzymatic polymerization [11], ion exchange by resin [2] and adsorption [12] but the most efficient process and economically feasible technology for removal phenol in adsorption, especially when using locally available adsorbent. Many research have studied the feasibility of inexpensive adsorbents such as Al-Khriet, (a powder which has been the legs of found in Typa Domingensis) agricultural waste and it is easily available in the waste could be alternative for cheaper an raw materials that are used to treat waste water. According to the literature there is no present study on the biosorptive removal of phenolic compound from aqueous solution using Al-Khriet. , they were selected for this research because they represent commonly encountrated phenolic pollutants in waste water treatment. The aim of this study is to look closely into the adsorption of Al-Khriet for removing phenol and 4-nitrophenol from aqueous solution. The effect of various factors, such as time of contact, bio sorbent dosage and initial adsorbent concentration the on adsorption process is investigated under batch experiments. Kinetic and equilibrium models were used to fit experimental data.

Material and Adsorbent Properties

Al-Khriet, a powder was collected from the marshes in the south of Iraq, first it was washed with dionized water several times to remove impurities and dried in air for two days before drying in oven at 100°Cover night finally Al-Khriet powder was stored in dictator.

Experimental Work

Different concentrations of phenol and 4-nitrophenol aqueous solution were prepared from stock of 500 mg/L by dissolving a proper amount of phenol and 4-nitrophenol in deionized water. The properties of phenol and 4nitrophenol are shown in Table 1.

Another reason for choosing these compounds is their difference in molecular structure; phenol is two dimensional, flat structures, while 4nitrophenol is three dimensional.

Table 1, Physical properties of adsorbents [13]

Adsorb ate	Phenol	4-nitrophenol
Molecular weight (g/mol.)	94.1	139.1
Water solubility (g/ L _{H2O})	93	17
Molecular dimensions, (A ⁰)	5.76*4.17	6.84*4.17

Adsorption was performed in a batch mode. The equilibrium isotherm was determined by mixing 0.5 gm of Al-Khriet with 25 ml of phenol and 4nitrophenol solution with different initial concentration (50-200) mg/L in conical flask. The flask was shaken in shaker at room temperature of 25°C for 3 hrs. Such a time is indeed to reach equilibrium according to series of experiments. The suspension of Al-Khriet was then filtered and the residual phenol concentration was measured by uv-visible (Shimadzu uv-160A) spectrophotometer. The latter was calibrated at a wavelength of 270 nm, 320 nm for phenol and 4nitrophenol respectively using a number of aqueous solutions of phenol 4-nitrophenol and at known concentration in order to calculate the calibration curve.

The adsorbed amount at equilibrium, $q_e (mg/g)$ and removal percentage of phenol and 4-nitrophenol onto Al-Khriet were calculated according to the following equation [14].

$$q_e = \frac{(C_0 - C_e)V}{w} \qquad \dots (1)$$

$$R\% = \frac{C_0 - C_e}{C_0} * 100 \qquad \dots (2)$$

Where R is the removal percentage, C_0 and C_e are the initial and equilibrium concentrations of adsorb ate (mg/L) respectively, V is the volume of solution (L), w is the weight of adsorbent used (gm.).

The adsorption kinetics was analyzed by adding 0.5gm of Al-Khriet to 25 ml of 50 mg/L of phenol and 4nitrophenol solutions. The sample was shaken and examined at different time intervals. The effect of adsorbent dosage and the initial concentration of feed solution were also studied by using different amount of adsorbent (0.2-1) gm for the 50 mg/L solution of phenol and 4-nitrophenol.

Results and Discussion Effect of Contact Time

As shown in Fig.1 the percent removal of phenol and 4-nitrophenol by adsorption onto Al-Khriet increases with contact time until attain equilibrium of about 3 hr. Removal percent equal to 91.5% and 82% for 4nitrophenol and phenol respectively at pH 6 and of 50 ppm ions concentration for each adsorb ate and 0.5 gm. of adsorbents. The result indicates that the rate of sorption of 4-nitrophenol and phenol on Al-Khriet were fast because of a largest amount of two compounds attached to the adsorbent within 1 hr of adsorption. The similar results have been reported by Khorsravi R. et al [15].

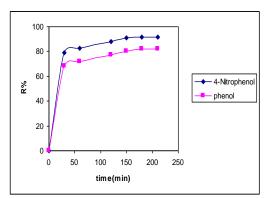


Fig.1 Effect of time on removal efficiency using Al-Khriet as adsorbent

The Effect of Adsorbent Dosage

The adsorption of phenol and 4nitrophenol on Al-Khriet was carried out by various adsorbent dosages. The relationship between adsorbent dosage and percent of removal is presented in Fig.2. It can be perceived the percent of removal increased with increasing of Al-Khriet dosage while the loading capacity q_e (mg/g) decreased, this is due to increase surface area, more adsorption sites are available. The optimum weight of adsorbents was found (0.5) gm. for Al-Khriet.

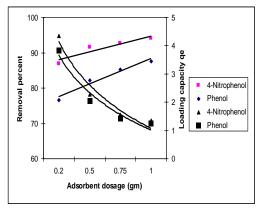


Fig.2 Effect of adsorbent dosage on percent removal for phenol and 4-nitrophenol by Al-Khriet, contact time 3 hr. initial concentration for both ions 50 ppm

It is appears from this figure that the removal percent of 4-nitrophenol is higher than phenol that is due to its lower water solubility and larger molecular weight of 4-nitrophenol when compared to phenol according to Table 1. In general, the adsorptive capacity was related to the electronwith drawing or electron- donating functional groups, water solubility of the compound and the molecular structure of the adsorb ate. The less soluble compounds are easier to be adsorbed [2].

Effect of Phenol and 4-nitrophenol Concentration

The effect of phenol and 4nitorphenol concentration on percent of removal was studied. The concentration was varied from (50-200) ppm on 0.5 gm. of Al-Khriet at room temperature. The result in Fig. 3 shows that the percent removal decreased as the concentration of phenol and 4-nitorphenol increased, indicating the less favorable sites and available for adsorb ate with increasing concentration. Removal percent equal to 85 % and 74% for 4-nitrophenol and phenol respectively at 200 ppm concentration, using 0.5gm of Al-Khriet and pH of 6. The pH value were 6 before and after mixing with adsorbent. 0.1M of NaOH and HCl were used for pH adjustment to fix the pH value in all experiments.

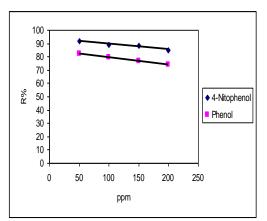


Fig.3 Removal of phenol and 4- nitro phenol using different concentration of ions

Kinetic Studies

Different kinetic models including the pseudo first order model (PFOM) and pseudo second order model (PSOM) were examined for the experimental data to estimate the adsorption kinetics. The PFOM and PSOM may be represented by the following equations respectively [16].

$$\ln(q_e - q_t) = \ln q_e - k_1 t \qquad \dots (3)$$

$$\frac{t}{q_t} = \frac{1}{k_2 {q_e}^2} + \frac{t}{q_e} \qquad \dots (4)$$

Where q_e , q_t is the amount of adsorbed at equilibrium (mg.g⁻¹), k_1 and k_2 is the rate constant for PFOM and PSOM respectively. The slope and intercept of plots $\ln(q_e-q_t)$ versus time were used to determine the k_1 while the slope and intercept of plot of $\frac{t}{q_t}$ versus t were used to calculate k_2 .

The PFOM and PSOM plots are shown in Fig. 4 and Fig. 5 respectively. A comparison of kinetics model is included in Table 2, based on their correlation coefficient (\mathbb{R}^2). The adsorption of phenolic compounds onto Al-Khriet is suitable for PSOM, based on higher correlation coefficients.

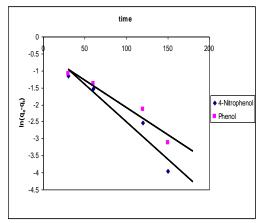


Fig.4 PFOM plots for phenol and 4nitrophenol

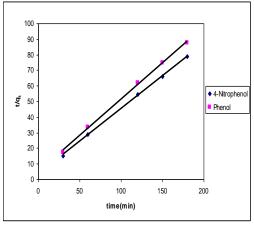


Fig.5 PSOM plots for phenol and 4-nitrophenol

for the kinetic models			
Kinetic model	Parameters	Nitrophenol	Phenol
PFOM	$k_1(min^{-1})$	0.022	0.016
	$q_{e}~(\mathrm{mg/g})$	0.733	0.613
	R_{1}^{2}	0.926	0.94
PSOM	$\begin{array}{c} k_2 (\text{mg.g}^{-1}.\\ \text{min}^{-1}) \end{array}$	0.055	0.048
	$q_e ~({ m mg/g})$	2.37	2.14
	R_1^2	0.999	0.998

Table 2, The rate constant and correlation coefficient for pseudo first and second order for the kinetic models

Equilibrium Isotherms

Langmuir (LM), Freundlich (FU) and Dubinin-Rodushkevich (D-RU) were chosen in this study to assess the relationship between the equilibrium concentration and the amount of phenol and 4-nitrophenol adsorbed on Al-Khriet. The LM assumes that the adsorption occurs at specific homogenous sites within the adsorbent and has found successful application in many studies of monolayer adsorption. The LM equation is given by the following equation [17].

$$\frac{C_e}{q_e} = \frac{1}{q_{\max}K_L} + \frac{C_e}{q_{\max}} \qquad \dots (5)$$

Where q_e is the solid phase adsorbate concentration in equilibrium (mg/g), q_{max} the maximum adsorption capacity corresponding to complete monolayer coverage (mg/g), C_e the concentration of adsorb ate at equilibrium (mg/L) and K_L is the Langmuir constant L/mg. The K_L and q_{max} can be evaluated from the slopes and intercept of linear plots C_e/q_e versus C_e as shown in Fig. 6, the parameter of these model were tabulated in Table (3).

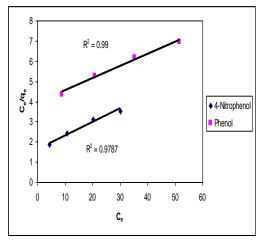


Fig.6, Adsorption isotherm of phenol and 4nitrophenol at pH (6) by using Langmuir

Table 3, Parameter of isotherms for phenol and 4-nitrophenol and correlation coefficient for Langmuir isotherm R^2

Kinetic model	Parameters	4- nitrophenol	phenol
Langmuir	$q_{ m max}$ (mg/g)	15.24	16.6
	K _L L/mg	0.0.039	0.015
	R^2	0.979	0.99

Freundlich model is present by following equation [18].

$$\ln q_e = \ln K_f + \frac{1}{n} \ln C_e \qquad \dots (6)$$

Freundlich describes the adsorption an energetically heterogeneous on which the adsorbed surface on molecules interactive. This are isotherm dose not predict any saturation of the sorbent by sorbate, indicating multilayer sorption where Freundlich K_{f} is the constant (mole/gm.) and n stands for the adsorption intensity. The value of K_{f} and 1/n were calculated from slope and intercept of the plot between $\ln q_e$ and $\ln C_{e}$ as shown in Fig. 7. The value of K_f and n were tabulated in Table (4).

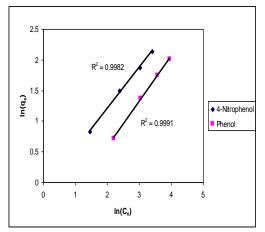


Fig.7 Adsorption isotherm of phenol and 4nitrophenol at pH (6) by using Freundlich

Table 4, parameter of isotherms for phenol and 4-nitrophenol and correlation coefficient for Freundlich isotherm R2

r reunanen isotnerni itz			
Kinetic model	Parameters	4- nitrophenol	phenol
Freundlich	$K_f \frac{mg}{g} \left(\frac{L}{mg}\right)^{\frac{1}{n}}$	0.886	0.414
	n	1.50	1.36
	R^2	0.998	0.999

The Dubinin-Rodushkevich model is an empirical equation employed to determine if the adsorption occurred by a physical or chemical process. The Dubinin-Rodushkevich[19] equation is more general than Langmuir because it does not assume a homogenous surface or a constant sorption potential. The linear form of this model is represented by

$$\ln q_e = \ln q_m - B\varepsilon^2 \qquad \dots (7)$$

B $(mol^2.Kj^{-2})$ is the constant related to sorption energy while ε is the polanyi sorption potential.

$$\varepsilon = RT \ln(1 + \frac{1}{C_e}) \qquad \dots (8)$$

R is the gas constant 8.314 $\text{J.mol}^{-1}\text{K}^{-1}$, T is the temperature in Kelvin. The value of B, q_m were calculated from the slopes and intercept of the plots $\ln q_e$ versus ε^2 as shown in Fig. 8 and 9 [19], the parameter of these models were tabulated in Table (5).

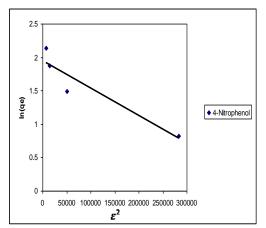


Fig.8 Adsorption isotherm of 4-nitrophenol at pH (6) by using Dubinin-Rodushkevich

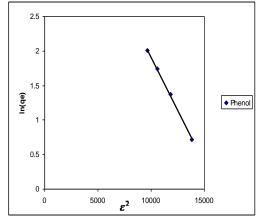


Fig.9 Adsorption isotherm of phenol at pH (6) by using Dubinin-Rodushkevich

Table (5) parameter of isotherms for phenol and 4-nitrophenol and correlation coefficient for Dubinin-Rodushkevich isotherm R^2

for Dublin Rodublike fren isotherm R			
Kinetic model	Parameters	4- nitrophenol	phenol
Dubinin- Rodushkevich	в*104	0.04	3
	<i>q</i> _{<i>m z</i>}	7	147.7
	\mathbb{R}^2	0.886	0.998

The experimental data yielded excellent fit within the following isotherm

FU>LM> D-RU

Based on its R^2 value as it gave the maximum R^2 value among the conceded model.

Conclusion

Al-Khriet can be used for first time effective. locally available as adsorbents for the removal of phenol and nitrophenol from waste water. The adsorption of phenol and nitrophenol on Al-Khriet is dependent on contact initial concentration time, and adsorbent dosage. It was observed that the removal process increase with contact time and attain equilibrium about 180 minute. In the study of kinetics of adsorption, the pseudosecond order mode provides better correlation than pseudo first order model. Also Freundlich model was found to fit the present experimental data with high correlation factor. Finally Al-Khriet under consideration is not only economical, but also an agriculture waste and locally available which would be useful for economical treatment of waste water containing phenol compounds.

References

1- Mahamad M.Ayad, Ahmed Abu El-Jaroslav stejskal, 2012. Nasr. Kinetics of methylene blue adsorption onto polyaniline nanotubes base/ silica composite, industrial Journal of and engineering chemistry. http://dx.doi.org/10-

1016/j.jiec.2012.05.012.

- 2- Nada vila, Siva Kumar and Kim Min, 2011, Removal of phenolic compounds from aqueous solution biosorption onto acetic acid leucocephala bark powder; equilibrium and kinetic. J.Chil. Chem.Soc. vol.56, no.1.
- 3- Gupta V.K., S., Sharma I.S. Yadav, D.Mohn. 1998, Utilization of bagasse fly ash generated in the sugar industry for the removal and of recovery phenol and pnitrophenol from waste water. J.Chem.Technol. Biotechnol.,71,pp. 180-186.

- 4- Spandre R., Dellonaco G-, 1996, Polyphenol pollution by olive mill waste waters, Tuscany, Italy, J.Environ.Hydrol., 4, pp. 1-13.
- 5- ATSDR (Agency for toxic substances and disease registry), 1998, Toxicological profile for phenol, US Department of health and human services, USA.
- 6- Hofman M. and Pietrzak R., 2012, Nitrogen-Doped carbonaceous materials for removal of phenol from aqueous solutions. The Scientific World Journal, V.2012, Article ID 297654, 8 pages, doi: 10. 1100/2012/297654.
- 7- Anirudhan T.S.. Sreekumari S.S., Bringle C.D., 2009, Removal of phenols from water and petroleum industry refinery effluents by activated carbon obtained from coconut coir pith adsorption. Pp. 439-451.
- 8- Leyva E., Moctezuma E., Ruiz M.G., Torresmatinez L. 1998, Photo-degradation of phenol by BaO.Li₂O-TiO₂ catalysts, catal,Today, 40,pp.367-376.
- 9- A.B. Pandit, P.R, Gogate, Mujumdar S., 2001, Ultrasonic degradation at 2:4:6 trichlorophenol in present of TiO₂ catalyst, ultrson, Sonochem, 8, pp. 227-231.
- 10- Shirgonkar I.Z., Pandit A.B., 1998, Sonophotochemical destruction of aqueous solution of 2, 4, 6 trichlorophenol, Ultrason, sonochem., 5, pp.53-61.
- 11- Buchanan I.D., Micell J.A., 1997, Peroxidase catalyzed removal of aqueous phenol, Biotechnol.Bioeng., 54, pp.251-261.
- 12- Burleigh M.C., Markowitz M.A., Spector M.S. Gaber, 2002, Porous poly-silsequioxanes for the adsorption of phenols. Eniron.Sci.Technol.36, pp.2515-2518.

- 13- Perry R.H., and Chilton C.H., 1973, Chemical Engineers Handbook, 5th edition, Mcgraw-Hill Kogakusha.
- 14- Daneshvar N., Aber S., Khani A., Khataee A.R., 2007. Study of imidaciopride removal from aqueous by adsorption onto granular activated carbon using an on-line spectrophotomatric system, J.Hazard. Mater. 144, pp.47-51.
- 15- Khosravi R., Moussavi G.R., Roudbar Mohammed Sh., 2011, Removal of high concentration of phenol from synthetic solutions by Fusarium Culmorum granules. Iran. J. Health and Environ., vol.4, no.4.
- 16- Soheil Aber, Alireza Khatee, Mohsen Sheydaei. 2009. Optimization of activated carbon fiber preparation from kenaf using K_2PO_4 as chemical activator for adsorption of phenolic compounds. Bioresource Technology, 100, pp. 6586-6591.

- 17- Pietrobelli, J.M.T., Modenus M.R., Fagundes-kten, F.R., Espinoza, 2009, cadmium copper and zinc biosorption study of nonliving jensa biomass water air soil pollut. 202, 385-392.
- 18- Patricia Uiretzky and Garolina Munoz, 2011, Enhancement metal removal from aqueous solution by fenton activated macrophyta biomass, desalination, 271, 20-28.
- 19- Saraswat S., Rai J.P.N., 2010, Heavy metal adsorption from aqueous solution using Eichhormia crassipes biomass, Int J. Miner process, 94, 203-206.