

Design of an adsorbent employing activated carbon fiber to remove lead

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Abstract: Zorflex® activated carbon fibers (ACF), reference FM100 198B, are used before and after an oxidizing procedure with H_3PO_4 to study the adsorption of Pb^{2+} . The point of zero charge was determined for the modified and unmodified fiber giving values of 2.3 and 4.3, respectively. After oxidizing the ACF, the fiber showed to have a greater Pb^{2+} adsorption capacity in comparison with the unmodified fiber, which is related with the acid sites increase, where lead was mainly adsorbed. Determination of the BET area was carried out by nitrogen physisorption at 77K. ACFs presented superficial areas between 1000 and 1500 m^2/g showing mostly, a microporous structure. The preliminary design of an adsorbent using the modified fiber is presented where the fiber superior physicochemical properties over the unmodified one are observed.

Keywords: isotherms; activated fibers; adsorbent; ion Pb^{2+}

Introduction

During the last decades, new alternatives and technologies showing adequate characteristics to reduce environmental pollution to a very low final level have been developed. Lead has been one of the most common contaminant target present in water streams and air. Alternatives such as the use of granular activated carbon (GAC), powdered activated carbon (PAC) and activated carbon fiber (ACF) have been widely implemented due to the increasing demand of this type of materials. Activated carbon fibers are one of the called “new materials” and, because of their characteristics, have been used for a wide range of applications, as in operation of air conditioning systems, in personal protection, for removing VOCs (benzene, acetone, dichloromethane, n-hexane, acrylonitrile, etc.) [1, 3] and, in the chemical industry, for the protection of wounds by semi-permeable band

aids that do not allow micro organisms access [1-10]. Activated carbon fibers offer several advantages in comparison with GACs and PACs. The ACF porous structure is mainly constituted by micropores, while other presentations of activated carbons have a complex structure formed by micropores, mesopores and macropores. The diameters of the ACFs are smaller (10-40 μm) than the sizes of GAC and PAC particles, providing a larger adsorption rate. Another advantage of the ACFs is that the distance among fibers may be controlled by selecting the precursor material to allow ACFs to be packed in bed fixed adsorbents.

In the same way, ACFs are excellent adsorbents due to their low pressure drop, high contact efficiency and flexibility, lightness and malleability. Additionally, they possess high porosity and consequently, huge superficial areas (950-1550 m^2/g), twice of the adsorptive capacity of GACs and are able

to adsorb elevated compounds quantities, as the above mentioned.

To design a efficient adsorption system, it is required to know the fundamental principles of the procedure of adsorption, of the material, the mass transfer rates, the transitions of the used bed, the changes produced as a consequence of the time and space during the adsorption process and the fiber behavior at equilibrium with the fluid phase, its saturation process and chemical and mechanical stability [1-39].

In the present work, it is presented the preliminary design of an adsorbent with different kinds of ACF's, for which lead adsorption isotherms on different kinds of ACFs are determined and the influence of the superficial characteristics of the fibers on the ACFs adsorptive capacity are studied.

Experimental details

Raw material

The Zorflex® fibers it has the advantages of having 100 % activate and 100 % carbon, faster adsorption kinetics, higher purity vapour uptake, smaller filtration beds and textile type properties.

Zorflex® fibers can also be impregnated with a range of chemicals of enhance the chemisorption capacity for selected gases.

The unmodified raw material showed to have low resistance to the tension with a crack load average of 0.011 KN and thickness of 0.60375 mm. The modified fiber showed an average of 0.022 KN and thickness of 0.589 mm. When compared to the Jean fiber, used in the textile industry, the raw fiber showed low resistance to cracking. Although not suitable for textiles, as an adsorbent these values are probably suitable.

Tests of Resistance

To the raw material, tests of mechanical resistance (tension) were carried out following the ASTM D5034 guideline. The crack load and thickness were determined by a preliminary analysis applied to four samples using an INSTROM and a LINEAR GAUGE BENSOR, respectively.

Impregnation with H_3PO_4 of the Activated Carbon Fibers

ACFs (Zorflex® fibers, ref. FM100 198B) were oxidized through a procedure similar to the one reported by Bandosz et al. [39]. In a 1L beaker, 20g of ACF and 500 mL of a 15% (v/v) H_3PO_4 solution, prepared with concentrated H_3PO_4 and deionised water, were added. The acid solution with the ACF was warmed for 2 h on an electric stove keeping the temperature below 50°C.

Table 1. Adsorbent specifications.

UNIT	1
IDENTIFICATION	AD-100
SERVICE	TO SAVE
USUALLY IN OPERATION	CONTINUOUS 24H
KIND	BED
FLUID	LIQUID
PROCESS DATA	
SUPPLY FLOW AT STP	
REAGENT QUANTITY AT STP	
WATER FLOW AT STP	
OPERATION TEMPERATURE °C	
MAXIMUM OPERATION PRESURE (Atm)	
MECHANICAL DATA	
PRESURE OF DESIGN (ATM)	1
TEMPERATURE OF DESIGN (°C)	25
MATERIALS OF CONSTRUCTION	STAINLESS STEEL
NUMBER OF FILTERS	5
LENGTH (cm)	40
pH	1 AT 13
INTERNAL DIAMETER (cm)	5,2

Afterwards, the solution was cooled down and filtered. The ACF was then washed several times using deionised water until the pH of the water was constant at 6. Finally, the ACF was dried on a stove at 110 °C for 24 h and was kept inside a dried and closed container.

Determination of the aqueous isotherms: Concentration vs. Lead adsorption time

Data were obtained for given quantity of fiber in a 250 mL erlenmeyer containing the Pb^{2+} solution of known concentration. The system was weighted at that point. The solution was thermostated and the solution was periodically stirred. At predefined time intervals, different samples of the solution were taken and the Pb^{2+} concentration was read by atomic absorption spectrophotometry using a PERKIN ELMER, model ANALYST 300 through a calibration curve previously prepared. The fiber and the solution were left in contact until the lead (Pb^{2+}) concentration in the fluid phase was constant. At predefined time intervals, different samples of the solution were taken and the Pb^{2+} concentration was read by atomic absorption spectrophotometry using a PERKIN ELMER, model ANALYST 300 through a calibration curve previously prepared.

Determination of Adsorption Isotherm in Aqueous Solution

ACFs were washed with distilled water to remove dust attained dust and dried at 110°C for 24 h. Afterwards, different quantities of fibers were submerged in lead solution at different concentrations and pH adjustment using 0.01 M HCl and NaOH solutions was performed every hour. Finally, samples from the solutions were taken after 24, 48 and 72 h and measured by atomic absorption spectrophotometry using a PERKIN ELMER, model ANALYST 300.

Determination of Active Sites

The concentration of active sites in the fibers was determined by the acid-base titration method proposed by Boehm [26]. Acid sites were neutralized with a 0.1 M NaOH standard solution and the basic sites with a 0.1 M HCl standard solution. The

active sites were determined gauging a 50 mL erlenmeyer with 0.1 M neutralizing solution and adding approximately 0.2 g of fiber. After three days, 10 mL aliquots were taken from the solution to determine acid sites by titration using 0.1 M NaOH was accomplished. Similarly, the basic sites were determined using 0.1 M HCl as titration agent.

Determination of Point of Zero Charge

The point of zero charge of the fiber (PZC) was determined through a process quite similar to the one reported by Babic et al [9]. In an erlenmeyer, 0.1 g accurately weighted of fiber and 20 mL of a 0.01M KCl and 0.004 M KOH solution were added. The solution was kept under stirring for 48h and the titration solution (0.1 M HCl) was slowly added, recording the added volume and the pH of the solution. On the other hand, the same procedure was carried out without using the fiber. The titration was achieved in accordance with the recommendations made by Leyva et.al. [7].

Characterization of the ACFs. N_2 Adsorption Isotherms at 77K.

Surface area and pore distribution were determined by the BET (Brunauer, Emmet and Teller) and DFT (Density Functional Theory) methods, respectively using a physisorption equipment QUANTACHROME INSTRUMENTS, model Autosorb 3B.

Breakage curves

Breakage curves were obtained by the same procedure alike to the one reported by Amaya, et al. [17-22].

Results and discussion

Characterization of the fibers

Raw material

In Figure 1 the Pb^{2+} adsorption behaviour on the fiber is shown. The equilibrium is attained after 4000 min with a concentration of 19.3 ppm, concentration permitted by the international environmental regulations, which allows a maximum concentration of 19.6 ppm [27-45]. There is an odd feature around 2000 min in the curve with eventual stirring which can be due to

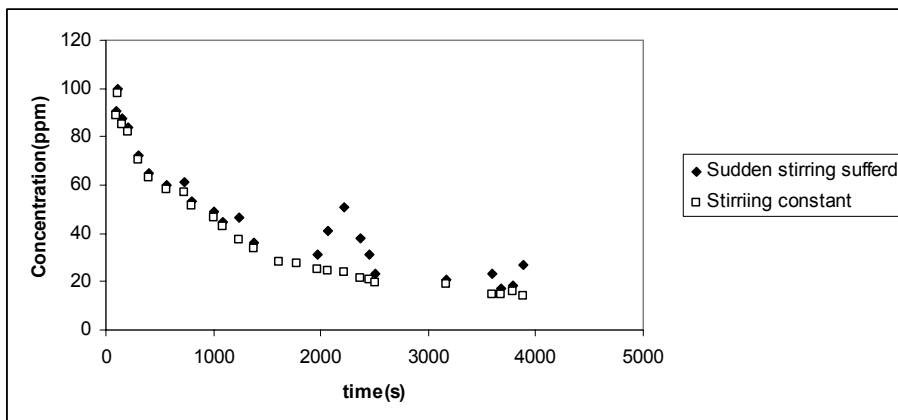


Figure 1. Curve of Concentration vs. Time for Lead Adsorption on Fiber.

some equilibrium perturbation by the sudden stir. The same figure also shows the curve with continuous stirring for comparison. This period allowed us to establish the experimentation time for the adsorption isotherms in aqueous solutions, point of zero charge and active sites.

Point of Zero Charge

As an amphoteric material, carbon surface displays groups of acid and basic character that control its behaviour in accordance with the medium. The carbons atoms of the basal plane edges may be combined in variable proportions with different heteroatoms, generating diverse superficial groups as shown in Figure 2. Most of these groups are oxygenated due to the tendency of the carbons to oxidize even at room temperature.

In the Figure 3, the schematic representation of the acid character of some oxygenated groups (carboxyls, hydroxyls and lactones) and of the oxygenated groups (pyrone, quinone and chromene type) is shown. [7]

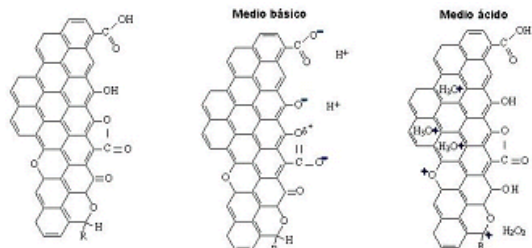


Figure 3. Oxygenated Groups (acid and basic character)

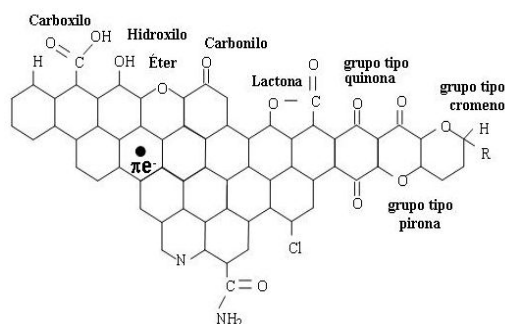


Figure 2. Schematic representation of the main superficial groups present on a carbon.

The acid and basic groups concentrations are equal in the point of zero charge and therefore the material is neutral. In order to achieve the maximum adsorption of certain pollutants, the carbon surface chemistry may be changed. The PZC of the ACFs was determined by plotting the pH of the solution against the volume of the titrating solution in the presence and in the absence of ACF. The pH where these two curves intercept corresponds to the PZC.

The PZC of the modified and unmodified fibers may be seen in figures 4 and 5. The obtained values, 4.3 and 3.2, respectively, show that both types of ACF have an acid character, weaker than the one reported by Rangel Mendez [43]. On the other hand, the PZC of the modified fiber is more acid than the one of the unmodified fiber and this is due to the higher proportion of acid

sites than basic sites because the treatment using H_3PO_4 introduced carboxylic groups.

The fact that the curves cross twice (4.3 and ~2.0) in the unmodified ACF means that the ACF impregnated with H_2PO_4 increase of acid groups.

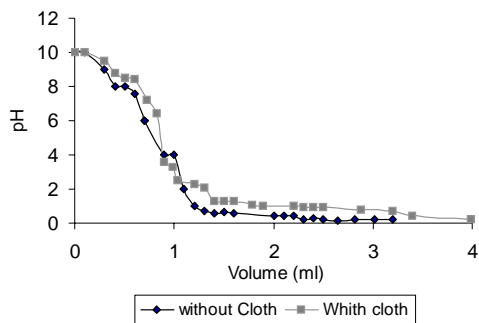


Figure 4. Point of zero charge (PZC) of the unmodified fiber.

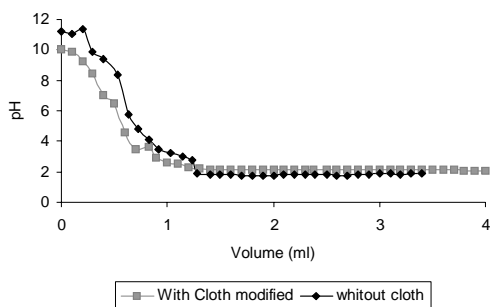


Figure 5. Point of zero charge (PZC) of the modified fiber.

Acid and basic sites

The curves obtained from the determination of acid and basic sites for the unmodified fiber are shown in figures 6 and 7.

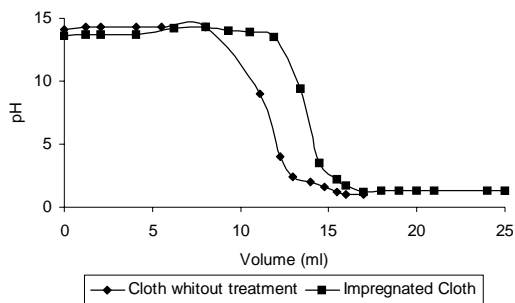


Figure 6. Acid Sites of the unmodified and impregnated fiber.

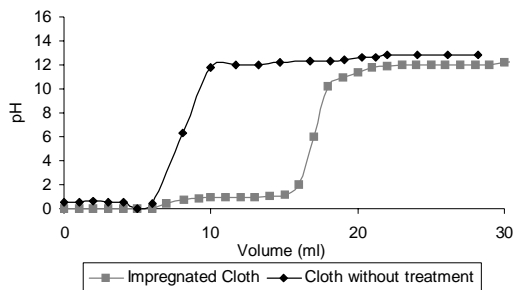


Figure 7. Basic Sites of the unmodified and impregnated fiber.

In figure 6, solutions of unmodified and impregnated fibers when they were titrated with NaOH are shown in a comparative way. It may be seen that with impregnation, fibers present higher quantity of acid groups than the unmodified fibers. This titration of graph, show that the acid of the impregnated fiber is weaker than the one of the unmodified ACF. When adding NaOH, this compound reacts with the acid sites of the ACF giving volume values of 10 and 13 mL for the unmodified and modified ACF, respectively. More volume on the impregnated fiber is required due to the greater acid sites concentration because of the treatment with phosphoric acid.

In Figure 7, it may be seen that the chemical treatment produces a slight slope depression indicating the presence of basic groups of weak character on the ACF surface. When adding HCl, this compound reacts with the basic sites of the ACF giving volume values of 6 and 16 mL for the unmodified and modified ACFs, respectively.

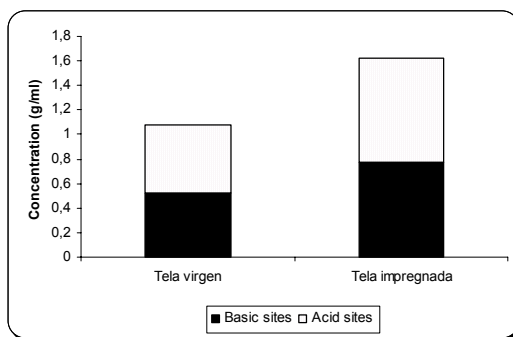


Figure 8. Active Sites Concentrations on ACFs.

Finally, in Figure 8 the concentration of the active sites of the unmodified and impregnated ACFs are shown. It is observed that the concentration of acid sites is slightly greater than the basic ones for both ACFs. These acid and basic sites concentrations are larger for the impregnated fiber because the chemical oxidation with H_3PO_4 increases the concentration of acid sites.

The concentrations of acid sites are 0.55 meq/g and 0.86 meq/g for the unmodified and the impregnated fiber, respectively and the concentration of basic sites are 0.52 meq/g and 0.77 meq/g, respectively, indicating that the ACFs surface is slightly acid.

The results show that the acid treatment does not modify strongly the superficial groups content of ACF.

It may be seen that the isotherms from aqueous solutions fit to the Langmuir's model.

Adsorption Isotherms from Aqueous Solution.

Experimental data from the isotherms of Pb^{2+} adsorption on the ACFs fitted using Langmuir's and Freundlich's models [11], mathematically represented as:

$$q = \frac{q_m KC}{1 + KC} \quad (5)$$

$$q = kC^{1/n} \quad (6)$$

It may be seen that the isotherms from aqueous solutions fit to the Langmuir's model, and that the ACFs produced I-type isotherms

since the increase at low concentrations is slightly pronounced and it agrees behaviors previously reported [49]. This type of isotherms is characteristic of the porous solids where the filling of micropores at low relative pressures is carried out. In the Table 2 show of parameters of fit to the model Langmuir's.

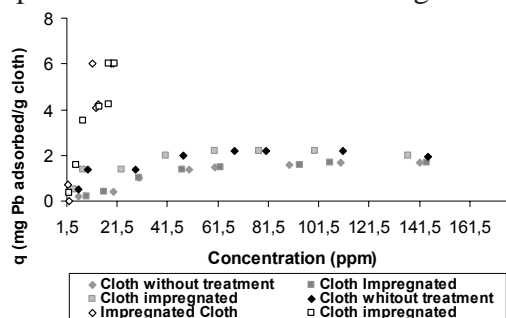


Figure 9. Isotherms from Aqueous Solution for the Pb^{2+} adsorption for different conditions.

Adsorption isotherms from Pb^{2+} aqueous solutions on unmodified and modified ACFs with adjusting pH to 5.0 and temperature at $25^\circ C$ are shown in Figure 9. It may be seen that the impregnated ACF has greater adsorption capacity than the unmodified ACF. The Pb^{2+} metallic cations in aqueous solutions adsorb more on the ACF acid sites and the major acid sites are the carboxylic, phenolic and lactonic [11]. This explains the previous result since the impregnated ACF has a greater acid sites concentration compared with the unmodified ACF.

It is important to note that the pH of the solution plays an outstanding role on the Pb^{2+} adsorption, the employed pH was taken from the lead speciation curve shown in Figure 10. It is considered that this pH change slightly modifies the results from figure 9 [29].

Table 2. Parameters of fit to the model Langmuir's

Sample	K	qmax	R	m	b
Cloth without treatment 72h	0.365	5.0916	0.9981	0.1964	0.538
Impregnated cloth 72h	0.0753	8.8652	1	0.1128	1.4975
Cloth without treatment 48h	0.1976	2.1677	0.9969	0.4613	2.3343
Cloth without treatment 24h	0.1273	1.9186	0.9982	0.5212	4.0923
Cloth impregnated 48 h	0.3667	2.1514	0.9907	0.4648	1.2673
Cloth impregnated 24 h	0.0591	1.8637	0.9968	0.5544	9.3723

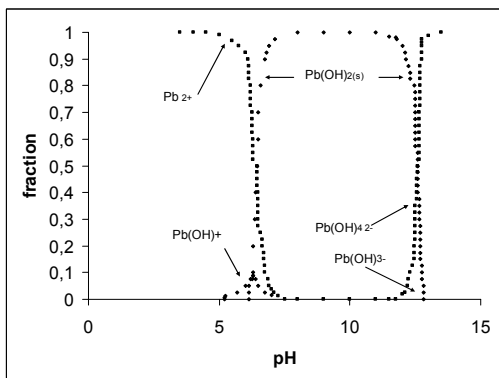


Figure 10. Lead Speciation Curve

Also, it can be observed that the capacity of the ACF for adsorbing Pb^{2+} increases when they are oxidized with H_3PO_4 solution. The adsorption increase is due to the augment of the acid sites concentration during the oxidation and to the fact that lead is mainly adsorbed on these.

N_2 Adsorption Isotherms

The surface area and the pore volume and average diameter are exhibited in the following figures for the unmodified and modified ACFs. These calculations were made through the BET and DFT methods.

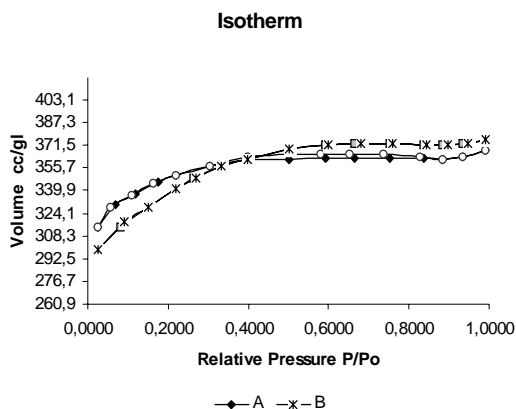


Figure 11. N_2 Adsorption isotherm for the unmodified and impregnated ACF.

In figure 11, the N_2 Adsorption isotherms at 77K for the unmodified and modified fibers are shown. In accordance to the IUPAC classification (International Union of Pure and Applied Chemists) classification,

the obtained isotherms are I-type and these are characteristic of the microporous solids, where filling of the smaller pores at very low pressures takes place. In figure 11-A, a small hysteresis cycle makes evident the presence of other pores different on the ACFs.

The surface areas of the unmodified and modified ACFs are $962m^2/g$ and $1014m^2/g$, respectively. The fiber, once is impregnated with phosphoric acid causes an increase in the superficial area and this is attributed to the oxidation process since involves a series of chemical reactions that eliminates some of the functional groups on the carbonaceous planes increasing the free space.

In Figure 12, the ACFs pore distribution by the DFT method is shown. The pore size distribution of the analyzed ACFs makes evident that these fibers are essentially supermicroporous suggesting, indicating that most of the pore volume is enclosed in pores with diameters smaller between 0.8nm and 2.0 nm.

From fig. 12-A, it may be seen that the pore volume of the impregnated fiber is greater than the one of the unmodified fiber due to the increase of contact time with H_3PO_4 solution. This increases the quantity of produced microporosity because there is a greater action from the activante material and a pore uncovering due to the reactions between the impregnant agent and the ACFs.

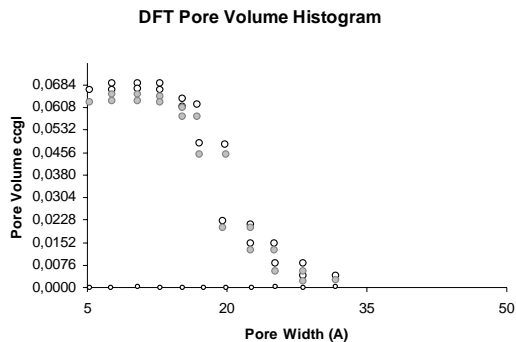


Figure 12. Pore distribution for unmodified and modified for ACF

Breakage Curves

For the interpretation of the solid-liquid interaction, it is necessary to take into account the adsorbate diffusion in the adsorbent particles. Fick's law is applied:

$$J = -D(c)dc/dx$$

Where J represents the adsorbent flux per unit of time and area, $D(c)$ corresponds to the diffusion coefficient, c is the concentration of the liquid phase in the adsorbent pores and x is the spatial coordinate.

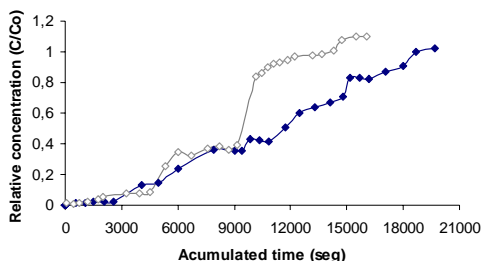


Figure 13. Breakage Curves for modified (A) and unmodified (B) for fiber.

As it may be seen in the figure 13, the concentrations of a fluid phase inside an ACF fixed bed varies proportionally with the change of position of the saturation front in the bed and with the time; the differences that appear between ACF treated and without treatment must fundamentally to the acid treatment. Once the fluid comes into contact with the fixed bed, most part of the mass transfer takes place near to the bed entrance. After a while, the solid becomes saturated and most part of the matter transfer takes place far from the entrance. Also, it can be observed that the impregnated fiber is a better adsorbent than the unmodified one because the saturation time is higher.

Scaling breakage curve for impregnated fiber.

The length of the mass transfer depends on the velocity of matter transfer, the velocity of the flow and the shape of the

equilibrium curve. The scale change of adsorbents is generally carried out from laboratory assays in a bed of small diameter that works with the same particle size and superficial velocity.

To make the scaling calculations, the breakage curve of the fiber impregnated with H_3PO_4 was used. An influent of 90.29 ppm in a burette with a capacity of 50 mL and a length of 14 cm was employed. The purpose is to achieve a scaling to a 40 cm long column. For the beginning times of the breakage curve, the output concentration is practically zero. Frequently, the breakage point is taken as a relative concentration of 0.05 or 0.1 and since only the last portion of treated fluid has the highest concentration, the solute fraction separated from the beginning to the breakage point is usually 0.95 or higher. Whether the adsorption continues beyond the breakage point, the concentration would increase quickly to approximately 0.5.

Values of u_0 of 0.2 cm s^{-1} , of \tilde{n}_{TCA} of 0.012 g cm^{-3} and C_0 of $4.366 \times 10^{-7} \text{ mol Pb}^{2+} \text{ cm}^{-3}$ were found.

Concentrations near 0.05 and 0.95 are going to afford breakage time, t_b of 1538.18 s and saturation time, t_s of 10403.19 s. The solute transference velocity, FA was calculated as $0.001074 \text{ mol Pb}^{2+} \text{ s}^{-1}$ and the breakage and saturation capacities as $q_b = 1.57 \text{ mg.g}^{-1}$ and $q_s = \text{mg.g}^{-1}$. The time when C/C_0 reaches the value of 0.5, t^* is 7215.61 s.

From these values, the Length without Using of the Bed, LUB, was found as 11.02 cm. The breakage time in these case, t_{b2} is 14958.54 s.

With these values, a curve representing the saturation behavior inside the bed, according with the time of a column of the desired (40 cm) was plotted (Figure 14, lefthand curve). Comparison of the two curves in Fig. 14 shows that the calculated and experimental curves are in a very good agreement.

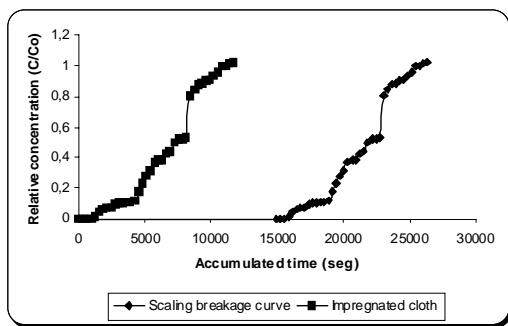


Figure 14. Curves of experimental breakage and scaling.

The design of the adsorbent is in Figure 15.

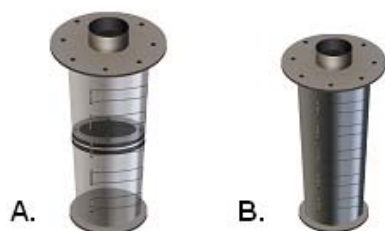


Figure 15. External and internal part of the adsorbent

Conclusions

The characterization of ACF by nitrogen physisorption indicated surface areas between 1000 and 1500 m²/g and that ACFs are mainly microporous materials. The pores of the ACFs are mainly microporous. The area of the impregnated ACF increases during the oxidation. The points of zero charge for the unmodified and modified fibers are 4.3 and 2.3, respectively, these are area acid due to the fact that ACFs have a larger concentration of acid than basic sites. The modified fiber became more acidic after the oxidation.

The impregnated ACFs presented a larger Pb²⁺ adsorption capacity than the unmodified ACF which is associated with the slight modification of groups by the acid treatment. The breakage curves allowed the appropriate adsorbent scaling. The breakage curve of the impregnated ACF was used for the design because it showed to have better

physicochemical properties than the unmodified ACF.

An adsorbent preliminary design was made using the breakage curves, with a length of 40 cm and a diameter of 5.2 cm. It is an experimental design that suggests that, in the future, a scaled version may be used.

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