

Removal of VOC from waste gas by an oil scrubber

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Removal of VOC from waste gas by an oil scrubber and the aqua clean system using oil instead of water was studied. Toluene, trichloroethylene and ethanol were used as VOCs. Soy bean oil, rape seed oil, high vacuum oil and turbo oil were used as oils. For comparison with VOC-oil system, ethanol – water system was also studied. VOC from waste gas was well removed by oil scrubber and the aqua clean system.

1. Introduction

Recently much attention has been paid to environment. Volatile organic compound (VOC) is used in many industries. In order to keep clean environment, VOC must be removed from waste gas. There are many methods for VOC treatment such as adsorption (Bandosz 2008, Zhao et al. 1998), combustion (Gervasini et al. 1996) and decomposition by ozone and electric discharge (Chang and Chang 2004). VOC can't be recycled by combustion and decomposition. The active carbon and zeolite are often used for adsorption of VOC. The active carbon and zeolite are good in the ability for adsorption of VOC, but they adsorb only little quantity of VOC. Therefore, the active carbon and zeolite are not suitable for removal of high concentration of VOC. It is expected that the oil scrubber can absorb high concentration of VOC and that VOC absorbed can be recycled. Moreover, it is expected that waste plant oil from homes can be used as an oil for the oil scrubber. Nippon SC developed the aqua clean system for treatment of smoke and exhaust gas from large kitchens of restaurants. The aqua clean system is an efficient water scrubber and is used to clean up smoke and exhaust gas from kitchens. In this work, removal of VOC from waste gas by oil scrubbers and the aqua clean system using plant oil instead of water was studied and the results were analyzed and discussed.

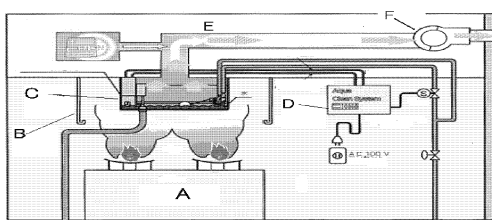


Fig.1 The aqua clean system in a kitchen.
A = range, B = hood, C = water scrubber,
D = water controller, E = duct, F = blower

2. The aqua clean system

Fig.1 shows a schematic diagram of the aqua clean system in the kitchen. The smoke from the range A is sucked into the water scrubber C and cleaned up. The aqua clean system can eliminate possibility of fire and remove bad fume and mists, because of use of water.

3. Experimental

Fig.2 shows a schematic diagram of the 3- stage oil scrubber. In Fig.2, A means air flow meter. B means vaporizer of VOC. C means oil scrubber. D and E mean gas sampling point at inlet and outlet of the oil scrubber, respectively. The scrubbers are made of 1dm³ messcylinder. Air at room temperature was used as a gas. Toluene, trichloroethylene and ethanol were used as VOCs. The concentration of VOC in the air was measured by FID or a handy VOC sensor (VOC-201H produced by Iable - Biott). Salad oil, rape seed oil, high vacuum oil and turbo oil were used as oils.

Fig.3 shows a schematic diagram of the aqua clean system used in this experiment. The dimension of the apparatus used was 65cm W x 60cm D x 100cm H. A means vaporizer of VOC. B means oil scrubber. C means filter. D means blower. The maximum flow rate of air is 13.1 m³ / min. The air which contained toluene was sucked into the shallow (about 7cm deep) salad oil bath B from the bottom of the oil scrubber by the blower. In the oil bath the air stirred up the oil like a shallow bubble column at large gas velocity and toluene was absorbed into the oil. All experiments were done at room temperature. The experimental conditions were $Q_G = 9.4 - 12.5$

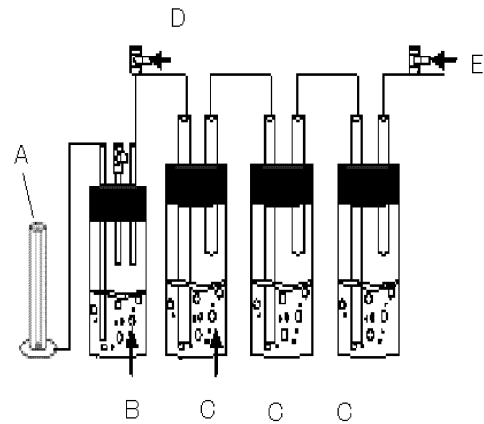


Fig.2 The 3-stage oil scrubber

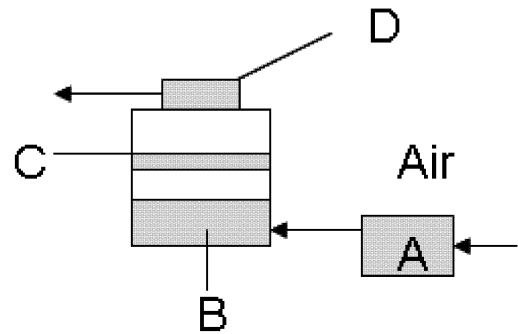


Fig.3 The aqua clean system used

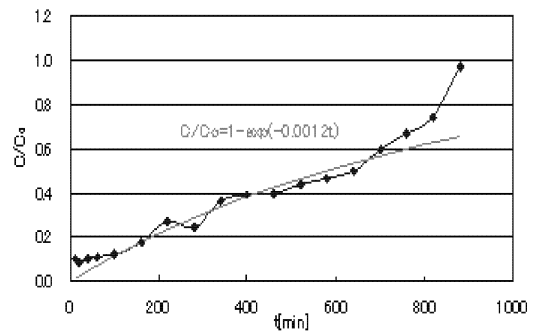


Fig.4 Toluene - soy bean waste oil system

m^3/min , $C_o=120\text{-}700$ ppm and $V_{oil}=16\text{-}22$ dm^3 . The depth of clear oil in the oil scrubber is in the range of 65 - 80mm. Q_G means flow rate of air. C_o and C mean concentration of VOC at inlet and outlet of the oil scrubber, respectively. V_{oil} means volume of oil. ppm means 10^{-6} mole fraction.

4. Experimental results and discussions

4.1 Toluene system

Fig.4 shows C / C_o for toluene-soy bean waste oil system by the 1-stage oil scrubber. The experimental conditions are $Q_G = 1.5$ L/min, $C_o = 11100$ ppm and $V_{oil} = 570$ mL. C / C_o increased with time.

Fig. 5 shows C / C_o for toluene-high vacuum oil system. C also increased with time. The experimental conditions are $Q_G = 1.5$ L/min, $C_o = 26300$ ppm and $V_{oil} = 570$ mL. C increased with t .

Fig.6 shows C / C_o for toluene-regenerated high vacuum oil. The experimental conditions are $Q_G=1.5$ L/min, $C_o=25900$ ppm and $V_{oil}=560$ mL. Removal of Toluene became worse than that by new oil.

Fig.7 shows C / C_o for toluene- rape seed oil system. The experimental conditions are $Q_G = 4$ L/min, $C_o = 2124$ ppm, $V_{oil} = 1524$ mL and the 3-stage oil scrubber. C/C_o was very low till at $t = 1000$ min. After at $t = 1000$ min, C/C_o increased rapidly with t .

Fig.8 shows C / C_o for toluene-turbo oil system by the 2-stage scrubber. The experimental conditions are $Q_G = 4$ L / min, $C_o = 6883$ ppm and $V_{oil} = 1242$ mL. C / C_o increased with t .

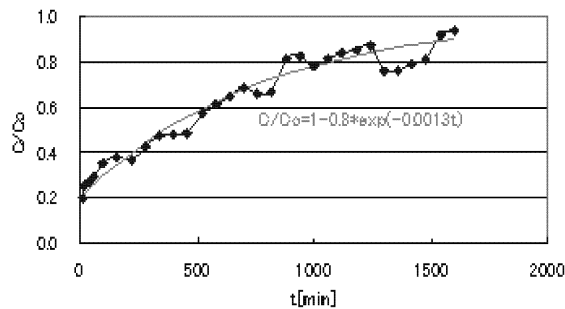


Fig.5 Toluene - high vacuum oil system by the 1-stage scrubber

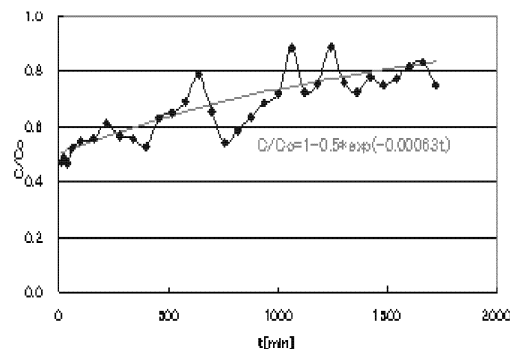


Fig.6 Toluene-regenerated high vacuum oil

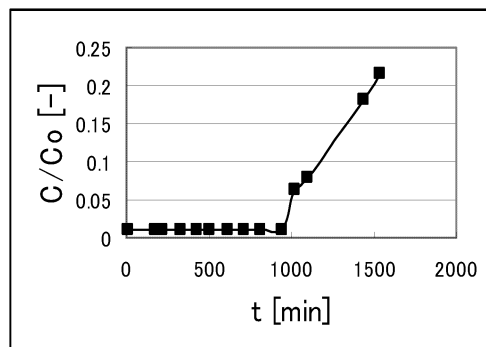


Fig.7 Toluene-rape seed oil system by the 3-stage oil scrubber

4.2 Trichloroethylene - soy bean oil system

Fig.9 shows C / C_o for the 1- stage trichloroethylene - soy bean oil system. The experimental conditions are $Q_G = 5$ L/m, $C_o = 211.3$ ppm and $V_{oil} = 540$ mL. C / C_o was nearly 20-30% till at 200 min and then increased rapidly with t .

Fig.10 shows C / C_o vs. t for the 3- stage trichloroethylene-soy bean oil system. The experimental conditions are $Q_G = 5$ L/m, $V_{oil} = 1590$ mL and $C_o = 307.5$ ppm. C/C_o was very low till at $t = 260$ min and increased rapidly with time.

Fig.11 shows volume V of liquid (= oil + trichloroethylene) in the oil scrubber. The experimental conditions are the same as those in Fig.10.

4.3 Ethanol – water system

For comparison with VOC-oil system, ethanol-water system was studied. Fig.12 shows C / C_o for the 1- stage ethanol - water system. The experimental conditions are $Q_G = 5$ L/m, $C_o = 211.3$ ppm and $V_{oil} = 540$ mL. C / C_o was nearly 15 % till at 1000 min and then increased rapidly with t . Fig.13 shows V vs. t . V increased with time. V means volume of (ethanol+ water).

4.4 Removal of toluene by the aqua clean system

Figs.14 and 15 show examples of the results. The horizontal axis means run number. The vertical axis means C [ppm]. Fig.14 shows the results for $C_{in} =$ about 200ppm, $H_{oil} = 65$ mm, $Q_G = 10.5$ m³ / min. The removal efficiency R was 40-41%.

Fig.15 shows the results for $C_{in} = 650$ -680ppm, $H_{oil} = 65$ mm, $Q_G = 10.5$ m³/min and $R = 51$ -53%. The removal efficiency of toluene is not so large. The reason why the removal efficiency is not so large may be because air flow rate is too large and oil scrubber is too shallow (60-80mm).

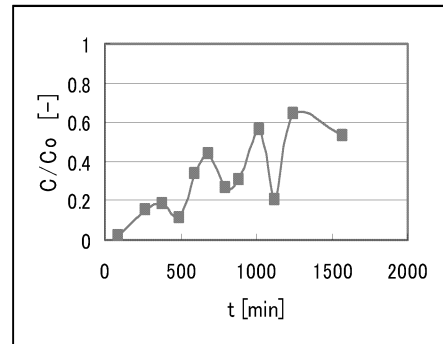


Fig.8 Toluene-turbo oil system by the 2 – stage oil scrubber

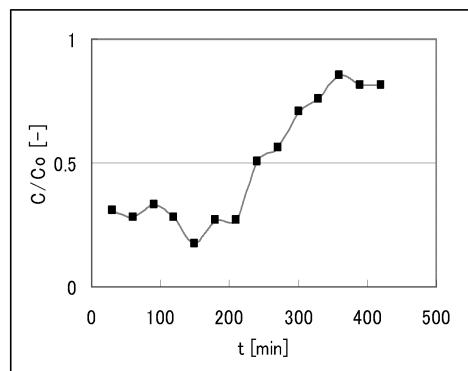


Fig.9 Trichloroethylene-soy bean oil by the 1-stage oil scrubber

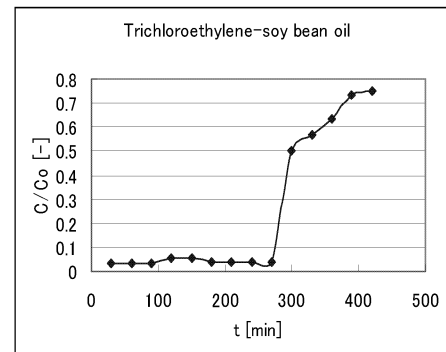


Fig.10 Trichloroethylene-soy bean oil by the 3-stage oil scrubber

Conclusion

- 1) Removal efficiency by the 3-stage oil scrubber was much larger than that by the 1-stage oil scrubber.
- 2) Removal efficiency was very large till at the critical time, however, after the critical time, the removal efficiency decreased.
- 3) Removal efficiency of toluene by the aqua clean system was nearly 50%.

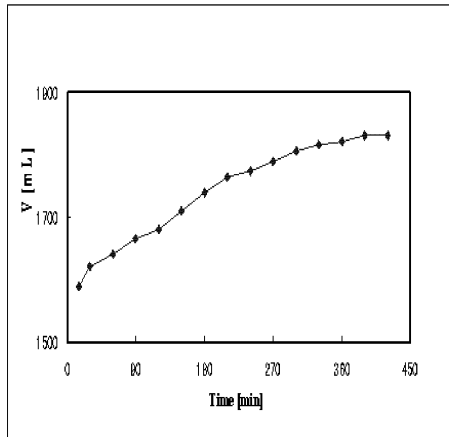


Fig.11 V vs. t for trichloroethylene-soy bean oil by the 3-stage oil scrubber
 $Q_G = 5 \text{ L/m}$, $V_{oil} = 1590 \text{ mL}$ and $C_o = 307.5 \text{ ppm}$

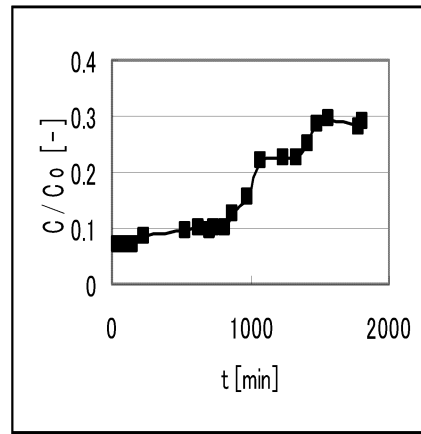


Fig.12 Ethanol - water system
 $Q_G = 5 \text{ L/m}$, $C_o = 211.3 \text{ ppm}$ and
 $V_{oil} = 540 \text{ mL}$.

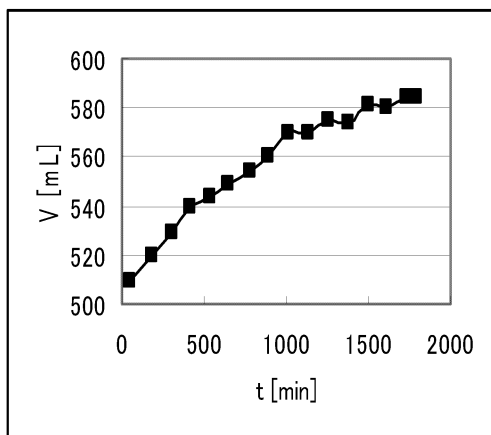


Fig.13 V vs. t for ethanol - water system
 The experimental conditions are the same as those in Fig.12.

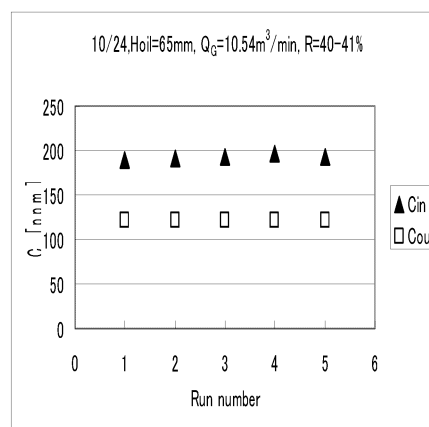


Fig.14 C vs. t for toluene - salad oil system by the aqua clean system.
 $C_{in} = \text{about } 200 \text{ ppm}$, $H_{oil} = 65 \text{ mm}$, $Q_G = 10.5 \text{ m}^3 / \text{min}$.

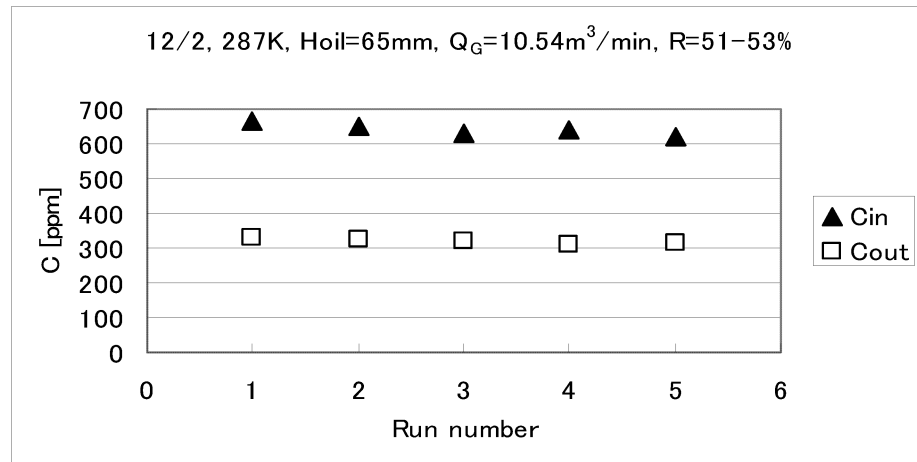


Fig.15 C vs. t for toluene – salad oil system by the aqua clean system.

Nomenclature

C = concentration of VOC in the air at outlet of oil scrubber or concentration [ppm]

C_o = concentration of VOC in the air at inlet of oil scrubber [ppm]

C_{in} = concentration of VOC in the air at inlet of oil scrubber [ppm]

C_{out} = concentration of VOC in the air at outlet of oil scrubber [ppm]

H_{oil} = depth of oil scrubber [cm]

Q_G = gas flow rate [L/min]

R = removal efficiency defined by $(1 - C_{out} / C_{in})$ [-]

t = time [min]

V = volume [mL]

V_{oil} = volume of oil [mL]

References

- Bandosz T. J., 2008, Chapter Twentyone-Removal of Inorganic Gases and VOCS on Activated Carbons, Adsorption by Carbons, Elsevier, 533-564
- Chang M. B. and Chang C.-C., 2004, Destruction and removal of toluene and MEK from gas streams with silent discharge plasmas, AIChE Journal, 43, 1325-1330
- Gervasini A., Vezzoli G. C. and Ragaini V., 1996, VOC removal by synergic effect of combustion catalyst and ozone, Catalysis Today, 29, 449-455
- Wang X. Daniels R. and Baker R.W., 2004, Recovery of VOCs from high-volume, low-VOC-concentration air streams, AIChE Journal, 47, 1094-1100
- Zhao X. S., Ma Q. and (Max) Lu G. Q., 1998, VOC Removal: Comparison of MCM-41 with Hydrophobic Zeolites and Activated Carbon, Energy & Fuels, 12, 1051-1054